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Unsteady Heat and Fluid Flow through a Curved Channel with Rectangular Cross-section for Several Cases of Aspect Ratio

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Abstract

In this paper, a comprehensive numerical study is presented for the fully developed two-dimensional flow of viscous incompressible fluid through a curved rectangular duct with different aspect ratios 2 and 3 for a constant curvature $\delta = 0.1$. Unsteady solutions are obtained by using a spectral method and covering a wide range of Dean number $100 \le Dn \le 1000$ and the Grashof number $1000 \le Gr \le 2000$. The outer wall of the duct is heated while the inner wall is cooled. The main concern of this study is to find out the unsteady flow behavior *i.e* whether the unsteady flow is steady-state, periodic, multi-periodic or chaotic, if the Dean number or the Grashof number is changed. For the aspect ratio 2, it is found that the unsteady flow is a steady-state solution for Dn = 100 and Gr = 100, 500, 1500, 2000 but periodic at Dn = 100 and Gr = 1000. If the Dean number is increased i.e. at = 500, it is found the unsteady flow is periodic at Gr = 1000, 1500 but chaotic at Gr = 100,500,2000. If the Dean number is increased further i.e. at Dn = 1000, the unsteady flow becomes chaotic for any value of Gr in the range. For the aspect ratio 3, however, it is found that the unsteady flow is a steady-state solution for Dn = 100 at Gr = 100 and Gr = 2000 but periodic at Dn = 100 and Gr = 500,1000,1500. If the Dean number is increased i.e. at Dn = 500 and 1000, the unsteady flow becomes chaotic for any value of Gr in the range. Contours of secondary flow patterns and temperature profiles are also obtained, and it is found that the unsteady flow consists of a single-, two-, three-, four-, five-, six-, seven- and eight-vortex solutions. It is also found that the chaotic flow enhances heat transfer more significantly than the steady-state or periodic solutions as the Dean number are increased.

Keywords: Curved rectangular duct; secondary flow; unsteady solutions; Dean number; Taylor number; Grashof number; time evolution.

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1. Introduction

Fluid flow through curved ducts and channels has been extensively studied over a wide range of applications because of their enormous applications in fluids engineering. Such motivation has provided a fairly comprehensive knowledge of physics and numerical modeling addressing intrinsic vortex-structure promoting mixing and momentum transfer. Now a days, flows in curved ducts channels are extensively used in many engineering applications, such as in turbo-machinery, refrigeration, air conditioning systems, heat exchangers, rocket engine, internal combustion engines and blade-to-blade passages in modern gas turbines. Dean [1] was the first who formulated the problem in mathematical terms under the fully developed flow conditions and showed the existence of a pair of counter rotating vortices in a curved pipe. The readers are referred to [2–5] for some outstanding reviews on curved duct flows.

The fluid flow in a rotating curved duct generates centrifugal and Coriolis force. Such rotating passages are used in many engineering applications e.g. in cooling system for conductors of electrical generators. For isothermal flows of a constant property fluid, the Coriolis force tends to generate vortices while centrifugal force is purely hydrostatic by (Zhang and his colleagues [6]). An early complete bifurcation study of two-dimensional (2-D) flow through a curved duct of square cross section was conducted by Winters [7]. He determined that the isolated symmetric 4-cell sub-branch is unstable while the isolated 2-cell sub branch is stable. The location of limit point and bifurcation points does not change much for curvature ratios less than 0.02, but at higher curvature ratios, they move to large Dn numbers. Mondal and his colleagues [8] performed comprehensive numerical study on fully developed bifurcation structure and stability of two-dimensional (2D) flow through a curved duct with square cross section and found a close relationship between the unsteady solutions and the bifurcation diagram of steady solutions. When a temperature induced variation of fluid density occurs for nonisothermal flows, centrifugal type buoyancy forces can contribute to the generation of vorticity [9]. These effects counteract each other in a non-linear manner depending on the direction of wall, resistance coefficients and the flow domain. Therefore, the effect of counteract of the system is more subtle and complicated and yields new; richer features of flow and heat transfer in general, bifurcation and stability in particular, for nonisothermal flows.

Time dependent analysis of fully developed curved duct flows was initiated by Yanase and Nishiyama [10] for a rectangular cross section. In that study, they investigated unsteady solutions for the case where dual solutions exist. The time-dependent behavior of the flow in a curved rectangular duct of large aspect ratio was investigated, in detail, by Yanase and his colleagues [5] numerically. They performed time-evolution calculations of the unsteady solutions with and without symmetry condition and showed that periodic oscillations appear with symmetry condition while aperiodic time variation without symmetry condition. Wang and Liu [11] performed numerical as well as experimental investigations of periodic oscillations for the fully developed flow in a curved square duct. Flow visualization in the range of Dean numbers from 50 to 500 was conducted in their experiment. They showed, both experimentally and numerically, that a temporal oscillation takes place between symmetric/asymmetric 2-cell and 4-cell flows when there are no stable steady solutions. Recently, Mondal and his colleagues [12] applied spectral method to study non-isothermal flow through a

curved rectangular duct of aspect ratios 1 to 3 and showed that the steady-state flow turns into chaotic flow through various flow instabilities if the aspect ratio is increased. They also showed that the chaotic solution becomes weak for small Dn's, while strong for large Dn's. However, solution structure as well as transient behavior of the unsteady solution is not yet resolved for the flow through a curved rectangular duct with bottom wall heating and cooling from the ceiling, which motivated the present study to fill up this gap.

One of the most important applications of curved duct flow is to enhance the thermal exchange between two sidewalls, because it is possible that the secondary flow may convey heat and then increases heat flux between two sidewalls. Chandratilleke and Nursubyakto [13] presented numerical calculations to describe the secondary flow characteristics in the flow through curved rectangular ducts that were heated on the outer wall, where they studied for small Dean numbers and compared the numerical results with their experimental data. Norouzi and his colleagues [14] investigated inertial and creeping flow of a second-order fluid with convective heat transfer in a curved square duct by using finite difference method. Chandratilleke and his colleagues [15] presented a numerical investigation to examine the secondary vortex motion and heat transfer process in fluid flow through curved rectangular ducts of aspect ratios 1 to 6. The study formulated an improved simulation model based on 3-dimensional vortex structures for describing secondary flow and its thermal characteristics. Zhang and his colleagues [16] adopted finite volume method and SIMPLE algorithm to perform laminar and turbulent flow through a curved square duct at low Reynolds number. There was a good agreement between their numerical result and the experimental data.

Recently, Mondal and his colleagues [17] investigated combined effects of centrifugal and Coriolis instability of the isothermal/non-isothermal flows through a rotating curved rectangular duct numerically. The secondary flow characteristics in a curved square duct were investigated experimentally by using visualization method by Yamamoto and his colleagues [18]. Three-dimensional incompressible viscous flow and heat transfer in a rotating U-shaped square duct were studied numerically by Nobari and his colleagues [19]. However, Unsteady Heat and Fluid Flow through a Curved Channel with Rectangular Cross-section for Various Aspect Ratios is not yet resolved. Very recently, Li and his colleagues [20] conducted a combined experimental and numerical study on 3D flow development in a curved rectangular duct with varying curvature. The flow fields were measured using Particle Image Velocimetry (PIV) and the numerical simulations were performed by solving the Reynolds Averaged Navier-Stokes (RANS) equations. Effects of curvature, Reynolds number and aspect ratio on Dean instability were discussed in that paper to accurately determine the core of secondary base vortices. To the best of the authors' knowledge, however, there has not yet been done any substantial work studying the solution structure as well as effects of unsteady solutions for the non-isothermal flow through a curved rectangular duct whose bottom wall is heated and cooling from the ceiling. But from the scientific as well as engineering point of view it is quite interesting because this type of flow is often encountered in engineering applications such as in gas turbines, metallic industry etc.

Examining the unique features of secondary flow and heat transfer, the main objective of the present study is to investigate time-dependent behavior of the unsteady solutions through a curved rectangular duct where outer wall of the duct is heated while the inner wall is cooled.

2. Flow Model and Mathematical Formulations

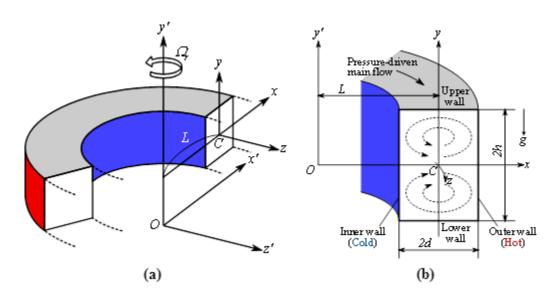


Figure 1: Coordinate system of the curved rectangular duct

Consider a hydro-dynamically and thermally fully developed two-dimensional (2D) flow of viscous incompressible fluid through a curved square duct, whose height or width are 2d. The coordinate system with the relevant notation is shown in Figure 1, where x' and y' axes are taken to be in the horizontal and vertical directions respectively, and z' is the axial direction. It is assumed that the lower (bottom) wall of the duct is heated while the upper (top) wall is cooled. The temperature of the lower wall is $T_0 + \Delta T$ and that of the upper wall is $T_0 - \Delta T$, where $\Delta T > 0$. It is also assumed that the flow is uniform in the axial direction, and that it is driven by a constant pressure gradient along the center-line of the duct. The dimensional variables are made non-dimensional by using the representative length d, the representative velocity $U_0 = \frac{\upsilon}{d}$, where υ is the kinematic viscosity of the fluid. We introduce the non-dimensional variables defined as

$$u = \frac{u'}{U_0}, \quad v = \frac{v'}{U_0}, \quad w = \frac{\sqrt{2\delta}}{U_0}w', \quad x = \frac{x'}{d}, \quad y = \frac{y'}{d}, \quad z = \frac{z'}{d}$$
$$T = \frac{T'}{\Delta T'}, \quad t = \frac{U_0}{d}t', \quad \delta = \frac{d}{L}, \quad P = \frac{P'}{\rho U_0^2}, \quad G = -\frac{\partial P'}{\partial z'}\frac{d}{\rho U_0^2}$$

where u, v and w are the non-dimensional velocity components in the x, y and z directions, respectively; t is the non-dimensional time, P is the non-dimensional pressure, δ is the non-dimensional curvature defined as $\delta = \frac{d}{L}$, and temperature is non-dimensional zed by ΔT . Henceforth, all the variables are nondimensionalized if not specified. Since the flow field is uniform in the z direction, the sectional stream function ψ is introduced as

$$u = \frac{1}{1 + \delta x} \frac{\partial \psi}{\partial y}$$
 and $v = -\frac{1}{1 + \delta x} \frac{\partial \psi}{\partial x}$ (1)

Then, the basic equations for w, ψ and T are expressed in terms of non-dimensional variables as

$$\left(1+\delta x\right)\frac{\partial w}{\partial t} + \frac{\partial(w,\psi)}{\partial(x,y)} - Dn + \frac{\delta^2 w}{1+\delta x} = (1+\delta x)\Delta_2 w - \frac{\delta}{1+\delta x}\frac{\partial \psi}{\partial y}w + \delta\frac{\partial w}{\partial x}$$
(2)

$$\left(\Delta_2 - \frac{\delta}{1+\delta x} \frac{\partial}{\partial x} \right) \frac{\partial \psi}{\partial t} = -\frac{1}{(1+\delta x)} \frac{\partial (\Delta_2 \psi, \psi)}{\partial (x, y)} + \frac{\delta}{(1+\delta x)^2} \left[\frac{\partial \psi}{\partial y} \left(2\Delta_2 \psi - \frac{3\delta}{1+\delta x} \frac{\partial \psi}{\partial x} + \frac{\partial^2 \psi}{\partial x^2} \right) - \frac{\partial \psi}{\partial x} \frac{\partial^2 \psi}{\partial x \partial y} \right]$$

$$+ \frac{\delta}{(1+\delta x)^2} \times \left[3\delta \frac{\partial^2 \psi}{\partial x^2} - \frac{3\delta^2}{1+\delta x} \frac{\partial \psi}{\partial x} \right] - \frac{2\delta}{1+\delta x} \frac{\partial}{\partial x} \Delta_2 \psi + w \frac{\partial w}{\partial y} + \Delta_2^2 \psi - Gr(1+\delta x) \frac{\partial T}{\partial x}$$

$$(3)$$

$$\frac{\partial T}{\partial t} + \frac{1}{(1+\delta x)} \frac{\partial (T,\psi)}{\partial (x,y)} = \frac{1}{\Pr} \left(\Delta_2 T + \frac{\delta}{1+\delta x} \frac{\partial T}{\partial x} \right)$$
(4)

where,

$$\Delta_2 \equiv \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2}, \quad \frac{\partial (T, \psi)}{\partial (x, y)} \equiv \frac{\partial f}{\partial x} \frac{\partial g}{\partial y} - \frac{\partial f}{\partial y} \frac{\partial g}{\partial x}$$
(5)

The equations for w, ψ and T are actually benefited for numerical computation. The non-dimensional parameters Dn, the Dean number; Gr, the Grashof number; and Pr, the Prandtl number, which appear in equation (2) to (4) are defined as:

$$Dn = \frac{Gd^3}{\mu\nu} \sqrt{\frac{2d}{L}}, Gr = \frac{\beta g \Delta T d^3}{\nu^2}, \quad \Pr = \frac{\nu}{\kappa}$$
(6)

where μ , β , κ and g are the viscosity, the coefficient of thermal expansion, the co-efficient of thermal diffusivity and the gravitational acceleration respectively is the viscosity of the fluid. In the present study, only Dn and δ are varied while Gr and Pr are fixed as, Gr = 100 and Pr = 7.0 (water).

The rigid boundary conditions for w and ψ are

$$w(\pm 1, y) = w(x, \pm 1) = \psi(\pm 1, y) = \psi(x, \pm 1) = \frac{\partial \psi}{\partial x}(\pm 1, y) = \frac{\partial \psi}{\partial y}(x, \pm 1) = 0$$
(7)

and the temperature T is assumed to be constant on the walls as

$$T(x,1) = 1, \quad T(x,-1) = -1, T(\pm 1, y) = y$$
(8)

There is a class of solutions which satisfy the following symmetry condition with respect to the horizontal plane y = 0.

$$w(x, y, t) \Rightarrow w(x, -y, t),$$

$$\psi(x, y, t) \Rightarrow -\psi(x, -y, t),$$

$$T(x, y, t) = -T(x, -y, t)$$
(9)

The solution which satisfies the condition (9) is called a *symmetric solution*, and that which does not an *asymmetric solution*. Note that, Equations (2) to (4) are invariant under the transformation of the variables

$$\begin{array}{l} y \Rightarrow -y \\ w(x, y, t) \Rightarrow w(x, -y, t), \\ \psi(x, y, t) \Rightarrow \psi(x, -y, t), \\ T(x, y, t) \Rightarrow -T(x, -y, t) \end{array}$$
(10)

Therefore, the case of heating the upper wall and cooling from the bottom can be deduced directly from the results obtained in this study.

3. Numerical Calculations

3.1. Method of numerical calculation

In order to solve the Equations (2) to (4) numerically, the spectral method is used. This is the method which is thought to be the best numerical method for solving the Navier-Stokes as well as energy equations [21]. By this method the variables are expanded in a series of functions consisting of the Chebyshev polynomials. That is, the expansion functions $\phi_n(x)$ and $\psi_n(x)$ are expressed as

$$\varphi_n(x) = (1 - x^2) \quad C_n(x),$$

$$\psi_n(x) = (1 - x^2)^2 \quad C_n(x)$$
(11)

where, $C_n(x) = \cos(n\cos^{-1}(x))$ is the n^{th} order Chebyshev polynomial. $w(x, y, t), \psi(x, y, t)$ and T(x, y, t) are expanded in terms of the expansion functions $\varphi_n(x)$ and $\psi_n(x)$ as:

$$w(x, y, t) = \sum_{m=0}^{M} \sum_{n=0}^{N} w_{mn}(t) \varphi_m(x) \varphi_n(y)$$
(12)

$$\psi(x, y, t) = \sum_{m=0}^{M} \sum_{n=0}^{N} \psi_{mn}(t) \psi_m(x) \psi_n(y)$$
(13)

$$T(x, y, t) = \sum_{m=0}^{M} \sum_{n=0}^{N} T_{mn}(t) \varphi_m(x) \varphi_n(y) - y$$
(14)

where M and N are the truncation numbers in the x and y directions respectively, and w_{mn}, ψ_{mn} and

 T_{mn} are the coefficients of expansion. To obtain the steady solution, the time derivative terms $\frac{\partial w}{\partial t}$, $\frac{\partial \psi}{\partial t}$, and $\frac{\partial T}{\partial t}$ are taken to be zero and the expansion series (12) - (14) with coefficients w_{mn} , ψ_{mn} and T_{mn} , being time independent, are substituted into the basic Eqs. (2), (3) and (4), and the collocation method (Gottlieb and Orszag, 1977) is applied. As a result, a set of nonlinear algebraic equations for w_{mn} , ψ_{mn} and T_{mn} are obtained. The collocation points (x_i, y_i) are taken to be

$$x_{i} = \cos\left[\pi\left(1 - \frac{i}{M+2}\right)\right], \qquad i = 1, \mathsf{K}, M+1$$

$$y_{j} = \cos\left[\pi\left(1 - \frac{j}{N+2}\right)\right], \qquad j = 1, \mathsf{K}, N+1$$
(15)

where i = 1, K, M + 1 and j = 1, K, N + 1. Steady solutions are obtained by the Newton-Rapshon iteration method assuming that all the coefficients to be time independent. To avoid difficulty near the point of inflection for the steady solutions, we use the arc-length method [22]. In the arc-length method, the arc-lengths play a central role in the formulation. The arc-length equation is

$$\sum_{m=0}^{M} \sum_{n=0}^{N} \left\{ \left(\frac{dw_{mn}}{ds} \right)^2 + \left(\frac{d\psi_{mn}}{ds} \right)^2 + \left(\frac{dT_{mn}}{ds} \right)^2 \right\} = 1$$
(17)

The convergence is assured by taking sufficiently small \mathcal{E}_p ($\mathcal{E}_p < 10^{-10}$) defined as

$$\mathcal{E}_{p} = \sum_{m=0}^{M} \sum_{n=0}^{N} \left[\left(w_{m\,n}^{(p+1)} - w_{m\,n}^{p} \right)^{2} + \left(\psi_{m\,n}^{(p+1)} - \psi_{m\,n}^{p} \right)^{2} + \left(T_{m\,n}^{(p+1)} - T_{m\,n}^{p} \right)^{2} \right].$$
(18)

Finally, in order to calculate the unsteady solutions, the Crank-Nicolson and Adams-Bashforth methods together with the function expansion (12) to (14) and the collocation methods are applied to equations (2) to (4).

3.2. Resistance coefficient

The resistant coefficient λ is used as the representative quantity of the flow state. It is also called the *hydraulic resistance coefficient*, and is generally used in fluids engineering, defined as

$$\frac{P_{1}^{*} - P_{21}^{*}}{\Delta_{z^{*}}} = \frac{\lambda}{d_{h}^{*}} \frac{1}{2} \rho \langle \omega^{*} \rangle^{2} (19)$$

where quantities with an P_1^* be asterisk denote dimensional ones, $\langle \rangle$ stands for the mean over the cross section of the duct and d_h^* is the hydraulic diameter. The main axial velocity $\langle \omega^* \rangle$ is calculated by

$$\langle \omega^* \rangle = \frac{v}{4\sqrt{2\delta l}} \int_{-1}^{1} dx \int_{-1}^{1} \omega(x, y, t) dy$$
 (20)

Since $(P_1^* - P_2^*) / \Delta_{z^*} = G$, λ is related to the mean non-dimensional axial velocity $\langle \omega \rangle$ as

$$\lambda = \frac{4\sqrt{2\delta}Dn}{\left\langle w\right\rangle^2}, (21)$$

where $\langle \omega \rangle = \sqrt{2\delta l} \langle \omega^* \rangle / v$. Equation (21) will be used to find the resistance coefficient of the flow evolution by numerical calculations.

4. Results and Discussion

In this study, we have investigated time evolution of the resistance coefficient λ for the fluid flows through a curved channel with rectangular cross-section for the curvature $\delta = 0.1$. We have studied the unsteady solutions of the flows at various Dean Numbers (*Dn*) for two cases of the aspect ratios; **Case I:** aspect ratio l = 2, **Case II:** aspect ratio l = 3. In addition to the time evolution of λ , the secondary flow patterns and temperature profiles at various Dean numbers are also discussed in detail.

4.1. Case I: Aspect Ratio l = 2

4.1.1. Time evolution of the unsteady solution

We investigate time evolution of λ for Dn = 100, 500 and 1000 over a wide range of the Grashof number Gr, $100 \leq Gr \leq 2000$ for aspect ratio l = 2. In this section, we present the unsteady solutions for Dn = 100 at Gr = 100,500,1500,2000, and we find that the unsteady flow is periodic for Dn = 100, Gr = 1000 and Dn = 500, Gr = 1000. We found that the unsteady flow is multi-periodic for Dn = 500 at Gr = 1500. We obtained the chaotic solution for Dn = 500 at Gr = 100,500,2000. We also obtained the chaotic solution for Dn = 1000 and Gr number varies from $100 \le Gr \le 2000$.

Time evolution of the resistance coefficient λ at time $20 \le t \le 30$ for Dn = 100 and Gr = 100, 500, 1500, 2000 for l = 2 are shown in Fig 3(a), 4(a), 6(a), 7(a) respectively. It is found that the flow is steady-state for these cases. Secondary flow patterns and temperature profiles are shown in Fig 3(b), 4(b), 6(b), 7(b) for Dn = 100 and Gr = 100, 500, 1500, 2000 respectively. Here it is seen that the solution oscillates between symmetric one and two vortex solutions. To draw the contours of ψ and T for the aspect ratio l = 2, we use the increments $\Delta \psi =$ 0.7 and $\Delta T = 0.2$, respectively. The same increments of ψ and T are used for all the figures in this study for l =2, unless specified. The right-hand side of each duct box of ψ and T is in the outside direction of the duct curvature. In the figures of the secondary flows, solid lines ($\psi \ge 0$) show that the secondary flow is in the counter clockwise direction while the dotted lines ($\psi < 0$) in the clockwise direction. Similarly, in the figures of the temperature field, solid lines are those for $T \ge 0$ and dotted ones for T < 0. We investigate time evolution of the resistance coefficient λ at time $20 \le t \le 40$ for Dn = 100 and Gr = 1000 as shown in Fig 5(a). We find that the flow is periodic for this case. From the contours of secondary flow and temperature profiles we observe that the unsteady flow is two-vortex solution, which is shown in Fig 5(b). In order to see the periodic oscillation more clearly, the phase space of the time evolution of λ is shown in Fig 5(c).

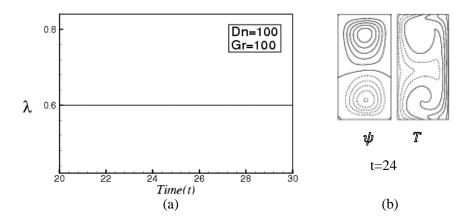


Figure 2: (a) Time evolution of λ at time $20 \le t \le 30$, (b) Secondary flow patterns (left) and Temperature profiles (right) for Dn = 100 and Gr = 100, l = 2 at time t = 24

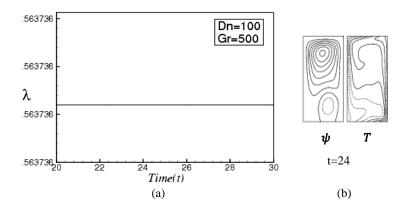


Figure 3: (a) Time evolution of λ at time $20 \le t \le 30$, (b) Secondary flow patterns (left) and Temperature profiles (right) for Dn = 500 and Gr = 100, l = 2 at time t = 24

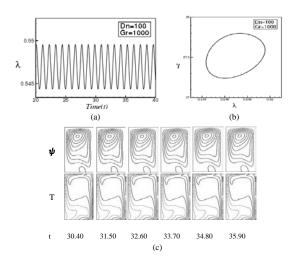


Figure 4: (a) Time evolution of λ at time 20 ≤ t ≤ 40, (b) Phase space for Dn = 100 and Gr = 1000, l = 2,
(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time 30.40 ≤ t ≤ 35.90.

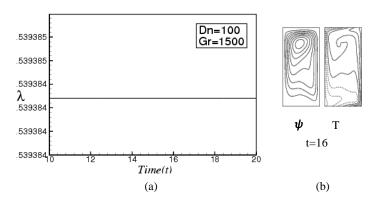


Figure 5: (a) Time evolution of λ at time $10 \le t \le 20$, (b) Secondary flow patterns (left) and Temperature

profiles (right) for Dn = 100 and Gr = 1500, l = 2 at time t = 16

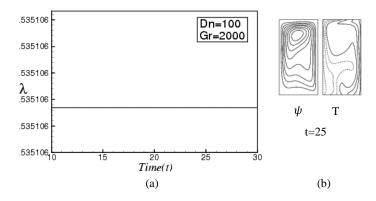


Figure 6: (a) Time evolution of λ at time $10 \le t \le 30$, (b) Secondary flow patterns (left) and Temperature profiles (right) for Dn = 100 and Gr = 2000, l = 2 at time t = 25

Time evolutions of λ for Dn = 500, Gr = 100 and Dn = 500, Gr = 500 are shown in Fig 8(a), 9(a) respectively. It is found the solution is chaotic for both the cases. Secondary flow patterns and temperature profiles are shown in Fig 8(b) and 9(b) respectively. As seen in Figs. 8(b) and 9(b), the unsteady flow is symmetric two-, three- and four-vortex solutions. In order to see the chaotic behavior more clearly, the phase space of the time evolution of λ is also obtained as shown in Figs. 8(c) and 9(c) respectively. It is found that the unsteady solution of the flow is periodic for Dn = 500 and Gr = 1000 at time $20 \le t \le 26$ as shown in Fig 10(a). Secondary flow patterns and temperature profiles are shown in Fig 10(b). We observe that asymmetric three-vortex solution is available. In order to see the periodic behavior more clearly, the phase space of the time evolution of λ is shown in Fig. 10(c). It is also found that the unsteady solution of the flow is multi-periodic for Dn = 500 and Gr = 1500 at time $27 \le t \le 29$ as shown in Fig. 11(a). Secondary flow patterns and temperature profiles are shown in Fig. 11(b). We observe asymmetric two vortex solutions for this case. In order to see the periodic behavior more clearly, the phase space of the time evolution of λ is obtained as shown in Fig. 11(c). Time evolution of the resistance coefficient λ at time $2 \le t \le 10$ for Dn = 500 and Gr = 2000 is shown in Fig. 12(a). We found that the flow is chaotic for Dn = 500 and Gr = 2000 at l = 2. Secondary flow patterns and temperature profiles are shown in Fig. 12(b). Here we found that there occur symmetric two- and three-vortex solutions. In order to see the chaotic behavior in more clearly, the phase space of the time evolution of λ is also shown in Fig. 12(c).

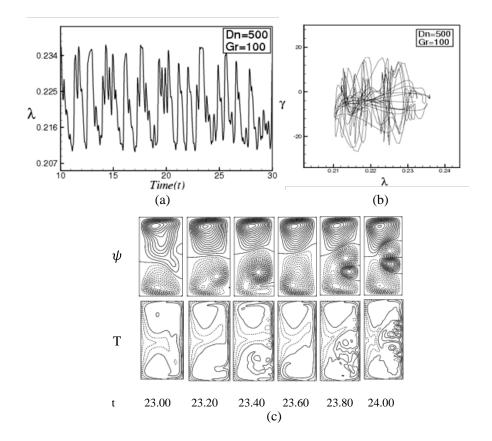


Figure 7: (a) Time evolution of λ at time 10 ≤ t ≤ 30, (b) Phase space for Dn = 500 and Gr = 100, l = 2,
(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time 23.00 ≤ t ≤ 24.00.

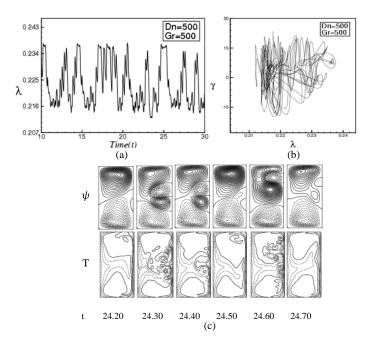


Figure 8: (a) Time evolution of λ at time $10 \le t \le 30$, (b) Phase space for Dn = 500 and Gr = 500, l = 2,

(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time 24.20 $\leq t \leq$ 24.70.

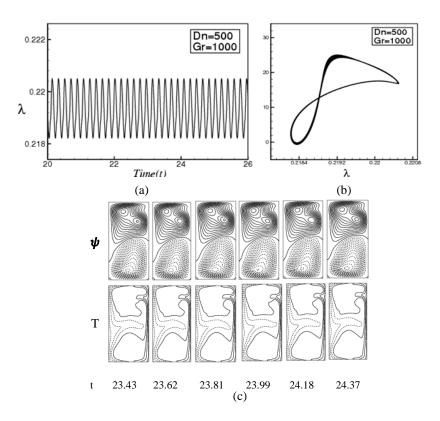


Figure 9: (a) Time evolution of λ at time 10 ≤ t ≤ 30, (b) Phase space for Dn = 500 and Gr = 1000, l = 2,
(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn,Gr and l at time 23.43 ≤ t ≤ 24.37.

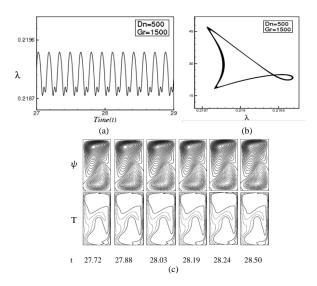
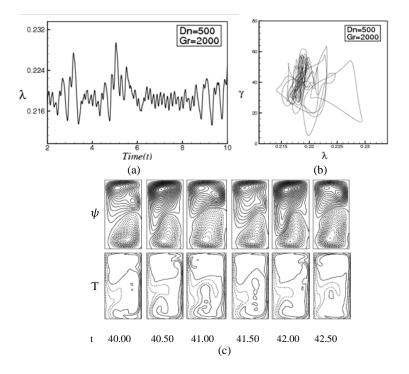


Figure 10: (a) Time evolution of λ at time 27 $\leq t \leq$ 29, (b) Phase space for Dn = 500 and Gr = 1500, l = 2, (c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for



same Dn, Gr and l at time 27.72 $\leq t \leq$ 28.50.

Figure 11: (a) Time evolution of λ at time $2 \le t \le 10$, (b) Phase space

for Dn = 500 and Gr = 2000, l = 2,(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time $40.00 \le t \le 42.50$.

Time evolution of the resistance coefficient λ at time $20 \le t \le 30$ for Dn = 1000 and Gr = 100 is shown in Fig. 13(a).We found that the solution is chaotic. Secondary flow patterns and temperature profiles are shown in Fig. 13(b). As seen in Fig. 13(b), the unsteady flow is symmetric five- and six-vortex solutions. In order to see the chaotic behavior more clearly, the phase space of the time evolution of λ is shown in Fig. 13(c). Unsteady solution of the flow is chaotic for Dn = 1000 and Gr = 500 at time $15 \le t \le 25$ is shown in Fig 14(a). Secondary flow patterns and temperature profile is shown in Fig 14(b), where we observe that the flow is asymmetric four-, five- and six-vortex solution. In order to see the chaotic behavior more clearly, the phase space of the time evolution of λ is also drawn as shown in Fig. 14(c). Time evolution of λ at time $10 \le t \le 20$ for Dn = 1000 and Gr = 1000, 1500 is shown in Fig 15(a), 16(a) respectively for the aspect ratio 2 and we find that the unsteady solutions are chaotic. Secondary flow patterns and temperature profiles are shown in Figs. 15(b) and 16(b) respectively. Here we found symmetric four-, five- and six-vortex solutions. We also drew the phase spaces of the time evolution of λ as shown in Figs. 15(c) and 16(c) respectively. It is found that the unsteady solution of the flow is chaotic for Dn = 1000 and Gr = 2000, l = 2 is shown in Fig. 17(a). Secondary flow patterns and temperature profiles are shown in Fig. 17(b), where we observe that the flow is an asymmetric four- and five- vortex solution. In order to see the chaotic behavior more clearly, the phase space of the time evolution of λ is obtained as shown in Fig. 17(c) for for Dn = 1000 and Gr = 2000, l = 2.

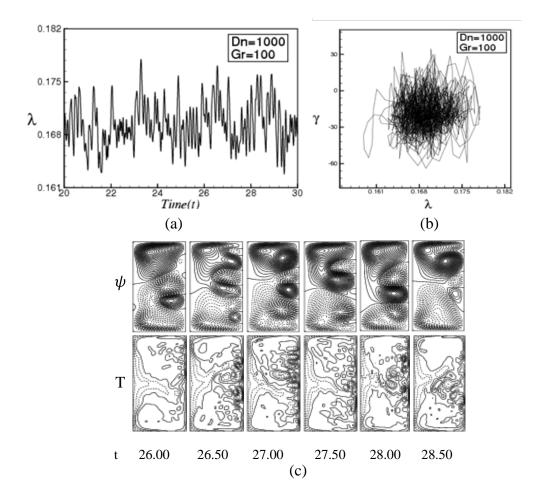


Figure 12: (a) Time evolution of λ at time 2 ≤ t ≤ 10, (b) Phase space for Dn = 1000 and Gr = 100, l = 2,
(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn,Gr and l at time 26.0 ≤ t ≤ 28.5.

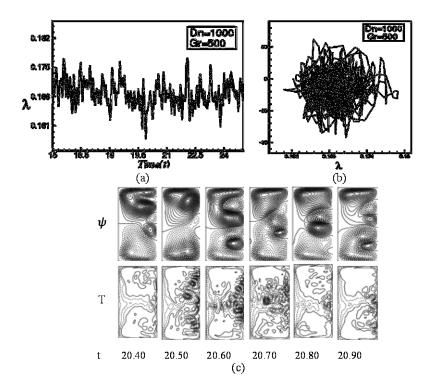


Figure 13: (a) Time evolution of λ at time 15 ≤ t ≤ 25, (b) Phase space for Dn = 1000 and Gr = 500, l = 2,
(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time 20.40 ≤ t ≤ 20.90.

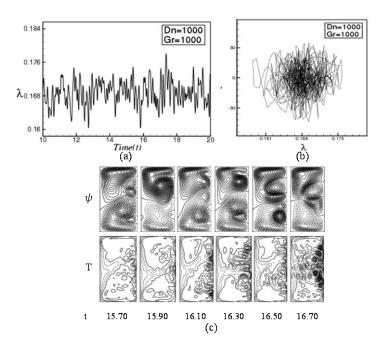


Figure 14: (a) Time evolution of λ at time $10 \le t \le 20$, (b) Phase space for Dn = 1000 and Gr = 1000, l = 2, (c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time $15.70 \le t \le 16.70$.

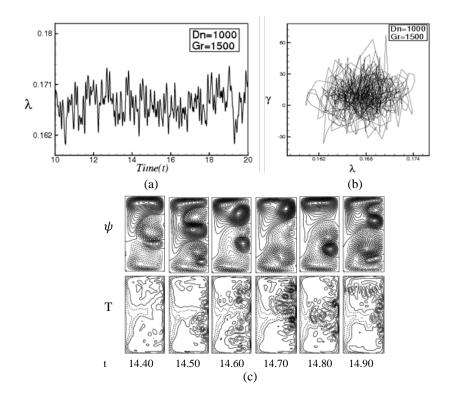


Figure 15: (a) Time evolution of λ at time $10 \le t \le 20$, (b) Phase space for Dn = 1000 and Gr = 1500, l = 2, (c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time $14.40 \le t \le 14.90$

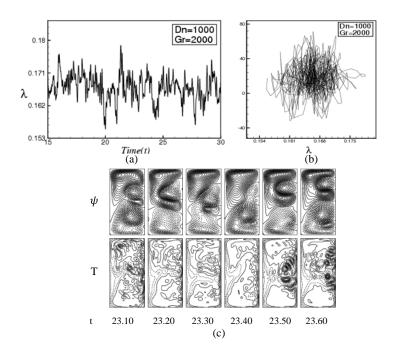


Figure 16: (a) Time evolution of λ at time $15 \le t \le 30$, (b) Phase space for Dn = 1000 and Gr = 2000, l = 2, (c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time $23.10 \le t \le 23.60$.

4.2. Case II: Aspect Ratio l = 3

4.2.1. Time evolution of the unsteady solutions

We investigate time evolution of λ for the Dean numbers Dn = 100, 500 and 1000 for the Grashof numbers $100 \le Gr \le 2000$ for aspect ratio l = 3. We obtained the steady state solution for Dn = 100 and Gr = 100, 2000. But at Dn = 100 and Gr = 500, 1000, 1500 the solution is periodic. We obtained the chaotic solution for Dn = 500 at $100 \le Gr \le 2000$. We also obtained the chaotic solution at Dn = 1000 for $100 \le Gr \le 2000$, l = 3.

Time evolution of the resistance coefficient λ at time $12 \le t \le 18$ for Dn = 100 and Gr = 100 is shown in Fig. 18(a). We found that the flow is a steady-state solution. Secondary flow patterns and temperature profiles are shown in Fig. 18(b). We observe asymmetric two vortex solution for this case. It is found that the unsteady flow is periodic for Dn = 100 and Gr = 500 at time $20 \le t \le 40$, which is shown in Fig. 19(a). Secondary flow patterns and temperature profile. are shown in Fig. 19(b). We observe that the flow is an asymmetric two-vortex solution. In order to see the periodic behavior more clearly, the phase space of the time evolution of λ is also obtained as shown in Fig. 19(c). Time evolution of λ at time $10 \le t \le 25$ for Dn = 100 and Gr = 1000 is shown in Fig. 20(a). It is found that the solution is multi-periodic oscillation. Secondary flow patterns and temperature profiles are shown in Fig. 20(b). Here we found asymmetric two-vortex solutions. In order to see the multi-periodic behavior more clearly, the phase space of the time evolution of λ is obtained as shown in Fig. 20(c). We find that the unsteady solution of the flow is periodic for Dn = 100 and Gr = 1500 as shown in Fig. 21(a). Secondary flow patterns and temperature profiles are shown in Fig. 21(b). We observe that the flow is an asymmetric two-vortex solution. In order to see the periodic behavior in more clearly, the phase space of the time evolution of λ as shown in Fig. 21(c). Time evolution of λ for Dn = 100 and Gr = 2000 is shown in Fig. 22(a).We found that the solution is steady-state solution. Secondary flow patterns and temperature profiles are shown in Fig. 22(b) for Dn = 100 and Gr = 2000. We observe asymmetric two-vortex solution for this case.

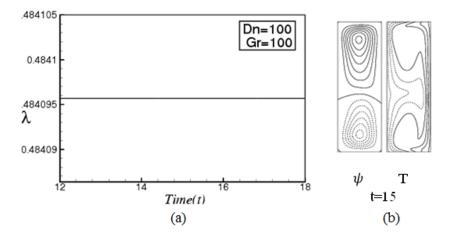
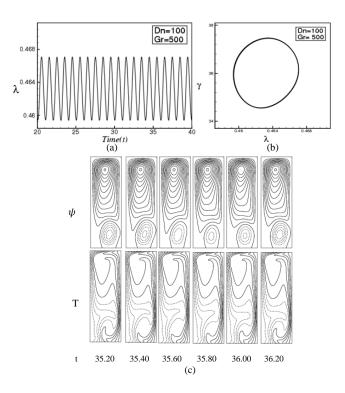


Figure 17: (a) Time evolution of λ at time $12 \le t \le 18$, (b) Secondary flow patterns (left) and Temperature



profiles (right) for Dn = 100 and Gr = 100, l = 3 at time t = 15

Figure 18: (a) Time evolution of λ at time 20 ≤ t ≤ 40, (b) Phase space for Dn = 100 and Gr = 500, l = 3,
(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time 35.20 ≤ t ≤ 36.20.

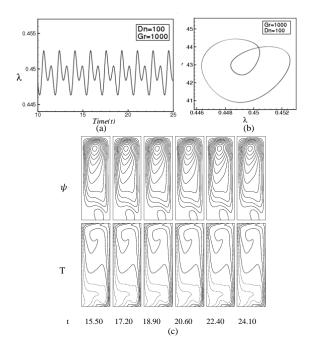


Figure 19: (a) Time evolution of λ at time $10 \le t \le 25$, (b) Phase space for Dn = 100 and Gr = 1000, l = 3, (c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for

same Dn, Gr and l at time $15.50 \le t \le 24.10$.

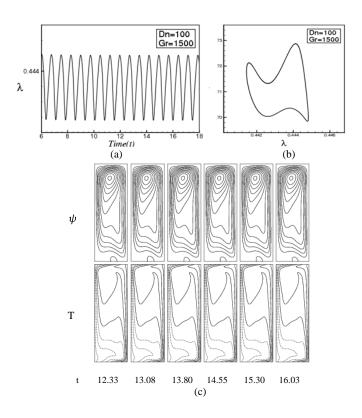


Figure 20: (a) Time evolution of λ at time 6≤ t ≤ 18, (b) Phase space for Dn = 1000 and Gr = 1500, l = 3,
(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn,Gr and l at time 12.33 ≤ t ≤ 16.03.

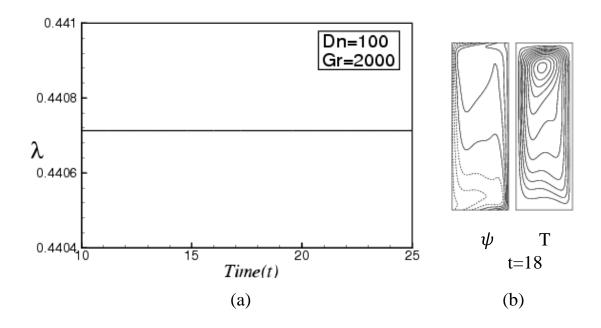


Figure 21: (a) Time evolution of λ at time $10 \le t \le 25$, (b) Secondary flow patterns (left) and Temperature

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profiles (right) for Dn = 100 and Gr = 2000, l = 3 at time t = 18.

Time evolution of the resistance coefficient λ at time 2.5 $\leq t \leq$ 9.5 for Dn = 500 and Gr = 100 is shown in Fig. 23(a). We found that the solution is a chaotic flow. Secondary flow patterns and temperature profile are shown in Fig. 23(b). Here we found symmetric four-, five- and six-vortex solutions. In order to see the chaotic behavior more clearly, the phase space of the time evolution of λ is shown in Fig. 23(c). It is found that the unsteady solution of the flow is chaotic for Dn = 500 and Gr = 500, which is shown in Fig. 24(a). Secondary flow patterns and temperature profile are shown in Fig. 24(b). We observe asymmetric three, four and five vortex solution. In order to see the chaotic behavior in more clearly, the phase space of the time evolution of λ as shown in Fig 24(c). Time evolution of the resistance coefficient λ at time $5 \le t \le 9$ for Dn=500 and Gr.=.1000 is shown in Fig. 25(a). We found that the solution is chaotic. Secondary flow patterns and temperature profile is shown in Fig 25(b). Here we found symmetric four-, five- and six-vortex solutions. In order to see the chaotic behavior more clearly, the phase space of the time evolution of λ is also drawn as shown in Fig. 25(c). Next, we obtained the unsteady solution of the flow and we find that the flow is chaotic for Dn = 500 and Gr = 1500 as shown in Fig. 26(a). Secondary flow patterns and temperature profile is shown in Fig 26(b). We observe that the flow is an asymmetric five-, six- and seven-vortex solution. In order to see the chaotic behavior more clearly, the phase space of the time evolution of λ is shown in Fig. 26(c). Then we calculate the unsteady solution of the flow for Dn = 500 and Gr = 2000 and we find that the flow is chaotic, which is shown in Fig. 27(a). Secondary flow patterns and temperature profile is shown in Fig 27(b). We observe that there occurs asymmetric five-, six- and seven-vortex solution. In order to see the chaotic behavior more clearly, the phase space of the time evolution of λ is also obtained as shown in Fig. 27(c).

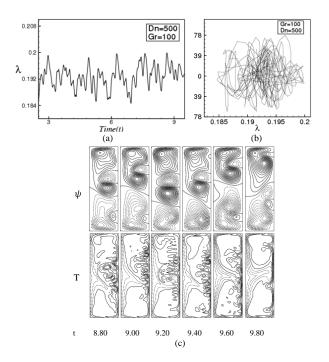


Figure 22: (a) Time evolution of λ at time $6 \le t \le 18$, (b) Phase space for Dn = 500 and Gr = 100, l = 3,

(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time $8.80 \le t \le 9.80$.

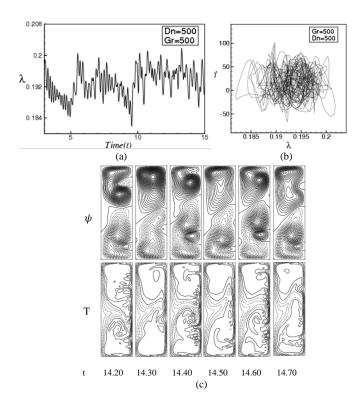


Figure 23: (a) Time evolution of λ at time 3 ≤ t ≤ 15, (b) Phase space for Dn = 500 and Gr = 500, l = 3,
(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time 14.20 ≤ t ≤ 14.70.

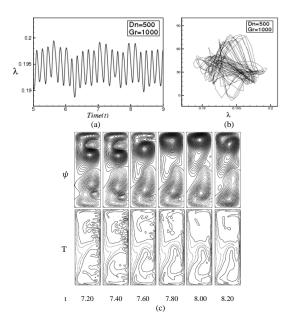
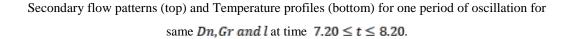


Figure 24: (a) Time evolution of λ at time $6 \le t \le 18$, (b) Phase space for Dn = 500 and Gr = 500, l = 3, (c)



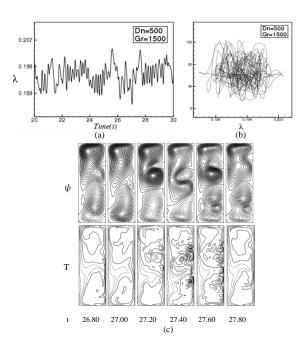


Figure 25: (a) Time evolution of λ at time 6≤ t ≤ 18, (b) Phase space for Dn = 500 and Gr = 1500, l = 3,
(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn,Gr and l at time 26.80 ≤ t ≤ 27.80.

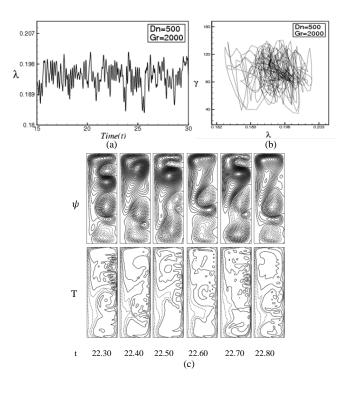


Figure 26: (a) Time evolution of λ at time $15 \le t \le 30$, (b) Phase space for Dn = 500 and Gr = 2000, l = 3,

(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time $22.30 \le t \le 22.80$.

Here we investigate time evolution of the resistance coefficient λ for Dn=1000 and Gr=100 as shown in Fig 28(a). We found that the flow is chaotic. Secondary flow patterns and temperature profile are shown in Fig. 28(b). Here we found symmetric five and six vortex solutions. In order to see the chaotic behavior more clearly, the phase space of the time evolution of λ is shown in Fig. 28(c). We investigate the unsteady solution of the flow for Dn = 1000 and Gr = 500 and it is found that the flow is chaotic as shown in Fig. 29(a) for time $0 \le t \le 17$. Secondary flow patterns and temperature profile are shown in Fig 29(b). We observe asymmetric six and seven vortex solution. In order to see the chaotic behavior in more clearly, the phase space of the time evolution of λ as shown in Fig 29(c). Time evolution of the resistance coefficient λ at time 30 $\leq t \leq$ 40 for Dn = 1000 and Gr = 1000, 1500 are shown in Figs. 30(a) and 31(a) respectively. We found that the solution is chaotic. Secondary flow patterns and temperature profile are shown in Fig 30(b) and 31(b) respectively. Here we found symmetric five, six and seven vortex solutions. In order to see the chaotic behavior in more clearly, the phase space of the time evolution of λ as shown in Fig 30(c) and 31(c) respectively. Unsteady solution of the flow is chaotic for Dn = 1000 and Gr = 2000 at time $15 \le t \le 35$ is shown in Fig 32(a). Secondary flow patterns and temperature profile is shown in Fig 32(b). We observe asymmetric five, six and seven vortex solution. In order to see the chaotic behavior more clearly, the phase space of the time evolution of λ is obtained as shown in Fig. 32(c).

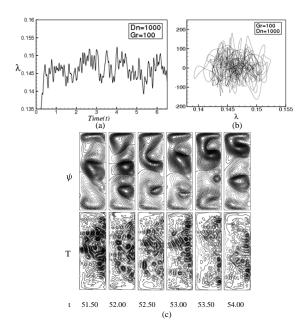


Figure 27: (a) Time evolution of λ at time $0 \le t \le 7$, (b) Phase space for Dn = 1000 and Gr = 100, l = 3,

(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time $51.50 \le t \le 54.00$.

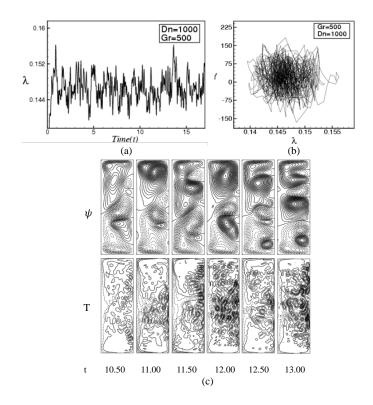


Figure 28: (a) Time evolution of λ at time $0 \le t \le 16$, (b) Phase space for Dn = 1000 and Gr = 500, l = 3,

(c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same *Dn*, *Gr* and *l* at time $10.50 \le t \le 13.00$ for l = -3.

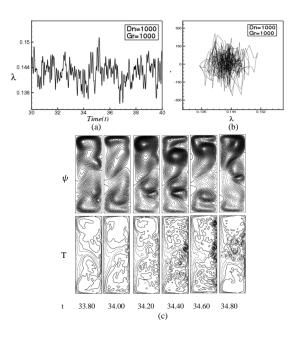


Figure 29: (a) Time evolution of λ at time $30 \le t \le 40$, (b) Phase space for Dn = 1000 and Gr = 1000, l = 3, (c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time $33.80 \le t \le 34.80$.

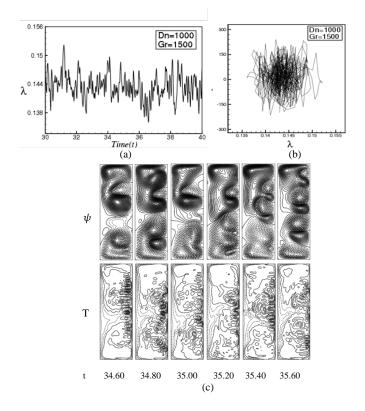


Figure 30(a): Time evolution of λ at time 30 $\leq t \leq$ 40 for Dn = 1000 and Gr = 1500 for the aspect ratio l = 3, (c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time 34.60 $\leq t \leq$ 35.60.

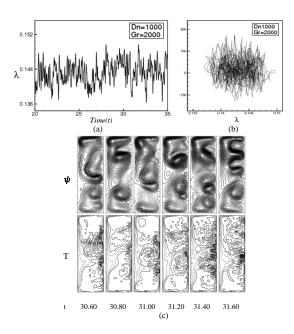


Figure 31(a): Time evolution of λ at time 20 $\leq t \leq$ 35 for Dn = 1000 and Gr = 1500 for the aspect ratio l = 3, (c) Secondary flow patterns (top) and Temperature profiles (bottom) for one period of oscillation for same Dn, Gr and l at time 30.60 $\leq t \leq$ 31.60.

4.2.2. Unsteady solutions in Dean vs Grashof Plane

Here, the distribution of the unsteady solutions, obtained by the time evolution calculations of the solutions, are presented in the phase diagram in the Dn-Gr plane for $0 < Dn \le 1000$ and $100 \le Gr \le 2000$ for the aspect ratios 2 and 3 in Figs. 33(a) and 33(b) respectively. In these figures, the circle denotes steady-state solution, the cross periodic solutions and the triangle chaotic solutions. As seen in Fig. 33(a), the steady-state solution turns into chaotic solution for small (Gr = 100, 500) and large Grashof numbers (Gr = 2000) for the case of aspect ratio 2, for moderate Grashof numbers, however, steady-state solution turns into chaotic solution, if the Dean number is increased. For the aspect ratio 3, we find that the steady-state solution turns into chaotic solution for Gr = 100, 500, 1500 and 2000, but at Gr = 1000, the steady-state solution turns into chaotic solution through periodic solution, if the Dean number is increased. Thus we get a through knowledge about the complete unsteady flow behavior of the present study from Figure 33.

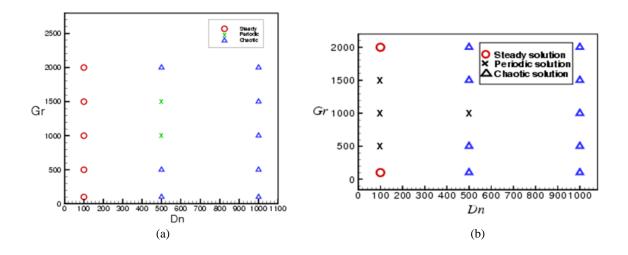


Figure 32: Graphical representation of unsteady solutions for $100 \le Dn \le 1000$ and $100 \le Gr \le 2000$ (a) for aspect ratio 2 and (b) for aspect ratio 3 respectively.

5. Conclusion

Here, we have studied a comprehensive numerical study of the time dependent solutions of the flow characteristics through a curved rectangular cross-section for various aspect ratios. Numerical calculations are carried out by using the spectral method over a wide range of the Dean number for a fixed curvature $\delta = 0.1$. In the present study, however, we performed time evolution calculations of the unsteady solutions through a curved rectangular flow for the aspect ratios 2, and 3.

In the present article, we studied the time-dependent solutions of the resistance coefficient λ over a wide range of the Dean number $100 \le Dn \le 1000$ for the rectangular cross-section of aspect ratio l = 2 and l = 3. At first, we investigated the unsteady solutions of the curved rectangular cross-section flow of aspect ratio l = 2. We found that the unsteady flow is steady-state for Dn = 100 at Gr = 100,500,1500,2000. But only the flow is periodic for Dn = 100 at Gr = 1000. We find that the unsteady flow is periodic for Dn = 500 and Gr = 1000. The unsteady flow is multi-periodic for Dn = 500 and Gr = 1500. It is also found that the solution is chaotic for Dn = 500 at Gr = 100, 500, 2000. Here we find that the flow is chaotic for Dn = 1000 at Gr number varies from $100 \le Gr \le 2000$. We obtained secondary flow patterns and temperature profiles for all types of solution and for the steady-state solution, we found two vortex solutions, while for the periodic flow, we obtained two vortex solution. In this regard, it should be noted that, the multi-periodic solution, obtained in the present study at the above-mentioned Dean numbers, they do not possess the same characteristics. When the flow is chaotic we get four- and five- vortex solution.

Then we studied the time evolution of λ for a wide range of the Dean number $100 \le Dn \le 1000$ and the range of Grashof Number $100 \le Gr \le 2000$ for the curved rectangular cross-section flow of aspect ratio 3 and we found that the unsteady flow is steady-state solution for Dn = 100 at Gr = 100,2000. However, the unsteady flow is periodic for Dn = 100 at. Gr = 500, 1000, 1500.

We found that the unsteady flow is chaotic for Dn = 500,1000 for all the grashof numbers investigated in this study. Contours of secondary flow patterns and temperature profiles are also obtained for all solutions. It is found that the periodic solution oscillates between asymmetric two-, and four-vortex solutions. When the flow is chaotic we get five, six and seven vortex solutions. The temperature distribution is consistent with the secondary vortices generated at the outer wall of the duct. It is found that the temperature passes significantly from the heated wall to the fluid as the secondary vortices increases.

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